# An Infrared Spectroscopic Study of the Re<sub>2</sub>O<sub>7</sub>/Al<sub>2</sub>O<sub>3</sub> Metathesis Catalyst

I. Physicochemical Properties, Structure, and Synthesis

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A new type of  $\text{Re}_2O_7/\text{Al}_2O_3$  catalyst has been prepared. Its optical properties, which are important in view of the experimental problems of *in situ* infrared spectroscopy of solid catalysts, are excellent. The carrier surface is completely covered with a monolayer of  $\text{Re}_2O_7$ . The spectrum of the calcined catalyst is characterized by hydroxyl bands at ca. 3500, 3640, and 3700 cm<sup>-1</sup> and by bands at 2000 and 1980 cm<sup>-1</sup>. At room temperature water is absorded mainly associatively; its infrared spectrum is characterized by a very broad band centered around 3100 cm<sup>-1</sup>. At higher temperatures dissociative adsorption occurs, giving two types of hydroxyl groups characterized by infrared bands at 3500 and 3640 cm<sup>-1</sup>. On reduction with hydrogen at 773 K a considerable amount of the  $\text{Re}_2O_7$  is reduced to metal; by X-ray spectroscopy rhenium metal crystals have been found. On subsequent oxidation with oxygen at 823 K the rhenium atoms are spread over the surface, reforming a monolayer of  $\text{Re}_2O_7$ .

#### INTRODUCTION

The metathesis reaction, known for a decade, has drawn much interest because of its technological and fundamental importance (1). A typical example is the exclusive formation of  $CH_2=CD_2$  when a mixture of  $CH_2=CH_2$  and  $CD_2=CD_2$  is exposed to a metathesis catalyst (2, 3):

$$\begin{array}{r} H_2C = CH_2 \\ + \longrightarrow 2H_2C = CD_2. \end{array}$$

Since it was recognized as a transalkylidenation reaction, little definite information has been obtained with regard to the reaction mechanism. Concerning the nature of the catalytic centers several authors conclude that partly oxidized transition metal ions seem to be necessary to bring about this reaction (4-6).

Most studies of the heterogeneously catalyzed metathesis have been carried out with or concern WO<sub>3</sub>/SiO<sub>2</sub>, MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>,  $MoO_3/CoO/Al_2O_3$  catalysts. The and present paper deals with the important  $Re_2O_7/Al_2O_3$  catalyst of which only in a few patents and papers information is published (1, 7). This catalyst is active even at subatmospheric pressures and at room temperature, and therefore particularly suited for an *in situ* infrared spectroscopic study: high temperatures and pressures, required by most other metathesis catalysts to effect metathesis, give rise to severe experimental difficulties. The infrared technique is valuable in that it enables one to observe the catalyst surface at a molecular level (8-10). At present infrared studies of metathesis catalysts have only been reported on a Mo(CO)<sub>6</sub>/Al<sub>2</sub>O<sub>3</sub> catalyst (11, 12). Owing to the complicated nature

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of that catalyst those studies did not give definite information with respect to metathesis activity (3, 13).

The results of our study will be presented in two parts. Part 1, the present paper, describes physicochemical properties of our  $\text{Re}_2\text{O}_7/\text{Al}_2\text{O}_3$  catalyst and the rather special technique of preparing a catalyst tailored to the demands of the infrared spectroscopic method. Gravimetry, electron microscopy and X-ray diffraction have been used to obtain information along with infrared spectroscopy. In Part 2, the succeeding paper (33), attention will be paid to the catalytic properties of the  $\text{Re}_2\text{O}_7/\text{Al}_2\text{O}_3$ catalyst, as well as to the interaction of alkenes with the catalyst surface.

#### METHODS

#### 1. The Catalyst

The main experimental difficulty of *in* situ infrared spectroscopy of heterogeneous catalysts is caused by conflicting demands on the properties of the catalyst sample. To obtain a satisfactory amount of catalyst surface in the infrared beam, a substantial optical thickness of the sample is required; however, to minimize scattering losses of the incident infrared beam a small optical thickness is needed. A successful and elegant compromise is reached by using catalysts with an aerogel structure as prepared by the method of Kistler (14). In their studies of Al<sub>2</sub>O<sub>3</sub> and SiO<sub>2</sub> Peri and Hannan (15, 16) have been the first to exploit the potentials of this technique for in situ infrared studies. The preparation of supported aerogel catalysts requires an extension of the technique of Kistler, such as for example Peri's method of preparing  $NiO/SiO_2$  aerogel catalysts (17).

We have been able to prepare effective and highly transparent  $MoO_3/Al_2O_3$ ,  $Mo(CO)_6/Al_2O_3$ ,  $WO_3/Al_2O_3$ , and  $Re_2O_7/Al_2O_3$ has been prepared by saturating a piece of alumina aerogel with the volatile  $Re_2O_7$  at temperatures between 773 and 873 K. This was effected by flushing a vessel containing rhenium powder and the aerogel with nitrogen at 773 K in order to dry the aerogel, followed by introducing oxygen at a temperature between 770 and 870 K. At these temperatures the rhenium is readily burned to the heptoxide. The aerogel piece had previously been cut into the dimensions required to fit the sample holder.

The Re<sub>2</sub>O<sub>7</sub> content, as determined by activation analysis, depended on the temperature at which the Re<sub>2</sub>O<sub>7</sub> was brought into contact with the carrier. The higher this temperature the lower the Re<sub>2</sub>O<sub>7</sub> content and it varied between 20 and 26 wt%. These catalysts had high specific surface area: e.g., the surface area of a 26% catalyst was 195 m<sup>2</sup>/g (BET, N<sub>2</sub>, 77 K). Optical properties were excellent. Transmission at 4000 cm<sup>-1</sup> was about 85%, while the optical density was approximately 80 mg/cm<sup>2</sup>.

The catalyst had to be stored in reduced form as its optical properties rapidly and irreversibly deterioriated on exposure to air, probably by water which is attracted due to the highly hygroscopic character of the carrier.

The Al<sub>2</sub>O<sub>3</sub> carrier was prepared following the method of Peri and Hannan (15, 16). Its specific surface area was 330 m<sup>2</sup>/g (BET, N<sub>2</sub>, 77 K) and according to spectrometric measurements the amounts of impurities (ppm) were Si ~ 100, Na < 100, Ca ~ 5, Fe ~ 10, Cu ~ 10, Mn < 1, and Mo ~ 0.5. X-Ray diffraction indicated a weakly crystalline  $\gamma$ -alumina.

### 2. Infrared Cell and Apparatus

The catalyst sample was mounted in a stainless steel holder which could be moved from an oven into the proper cell by means of a winch. The cell had an optical path-length of 10 mm. A reference cell with the same optical pathlength could be connected with the measuring cell. Condensable gases could be trapped in a cold

finger. By means of a conventional mercury diffusion pump and cold traps a dynamic vacuum could be reached of  $2.6 \times 10^{-8}$  Pa. Details are given elsewhere (3). Grubb-Parsons Mk III and Perkin–Elmer 337 double beam spectrophotometers have been used to obtain the spectra. At times an optical wedge in the reference beam was necessary. Owing to the good optical properties of the samples normal split programs could be used. For the spectra taken with the Grubb-Parsons apparatus the accuracies of the indicated wavenumbers are  $3 \text{ cm}^{-1}$  and for those taken with the Perkin–Elmer apparatus 5  $cm^{-1}$ . The latter spectra are marked with PE. When the Grubb–Parsons spectrophotometer was used with standard instrument adjustments, the sample was heated to about 333 K by the infrared beam. To prevent extensive heating of the sample this instrument was operated in certain cases with a reduced source intensity. This is critical when recording spectra of adsorbed species in the presence of gaseous reactants, as a hot sample heats the gases in the measuring cell, resulting in a difference in optical densities of the gases in the two cells.

#### 3. Other Techniques

Samples for transmission electron microscopy were cut with an LKB ultramicrotome from catalysts embedded in polymethylmethacrylate; the thickness of the sections was between 4 and  $5 \times 10^{-8}$  m.

Gravimetric data were obtained with a Cahn RG balance.

## 4. Materials

 $^{18}O_2$  was obtained from I.C.N. Its purity was 98%. D<sub>2</sub>O (Fluka) had a purity of 98% and the rhenium powder, also from Fluka, contained 0.1% impurities (these values have been given by the manufacturers).

#### RESULTS

## 1. Infrared Spectrum of the Re<sub>2</sub>O<sub>7</sub>/Al<sub>2</sub>O<sub>3</sub> Catalyst

Figure 1 shows the infrared spectra of  $\operatorname{Re_2O_7/Al_2O_3}$  (23%  $\operatorname{Re_2O_7}$ ) and of the carrier  $\operatorname{Al_2O_3}$ . Both spectra were obtained



FIG. 1. The infrared spectra of (a)  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and (b) Re<sub>2</sub>O<sub>7</sub>/Al<sub>2</sub>O<sub>3</sub>. In both cases the samples have been outgassed for 1 hr at 823 K. The marks I, II and III indicate different hydroxyl groups of the Re<sub>2</sub>O<sub>7</sub>/Al<sub>2</sub>O<sub>3</sub> catalyst surface.



FIG. 2. The infrared spectrum of the deuteroxyl groups on a deuterated  $\text{Re}_2O_7/\text{Al}_2O_3$  catalyst.

after treating the samples with oxygen  $(13 \times 10^3 \text{ Pa})$  at 823 K for 1 hr, followed by 1 hr pumping at the same temperature; this procedure is the standard calcination procedure.

In the hydroxyl region of the spectrum alumina hydroxyl bands at 3700, 3780, 3800, and 3740 cm<sup>-1</sup> are observed. This spectrum closely resembles spectra of



Fig. 3. The relative amounts of different hydroxyl groups as a function of the  $\text{Re}_2\text{O}_7$  content of the catalyst. (a) 26%, (b) 23% and (c) 20%.



FIG. 4. The effect of  ${}^{16}O{-}^{18}O$  exchange on the bands at 2000 and 1980 cm<sup>-1</sup>. (a) Re<sub>2</sub>  ${}^{16}O_7/Al_2O_3$  and (b) Re<sub>2</sub>  ${}^{18}O_7/Al_2O_3$ .

alumina obtained by other authors (10, 18). The spectrum of Re<sub>2</sub>O<sub>7</sub>/Al<sub>2</sub>O<sub>3</sub> shows in this region three bands at 3700 (I), 3640 (II), and 3500 cm<sup>-1</sup> (III). To clarify the origin of these bands H–D exchange was effected. From the spectrum of the deuterated metathesis catalyst it can be concluded that there are three different types of hydroxyl groups (Fig. 2).

Figure 2 shows bands at 2730 (I), 2685 (II) and 2595 (III) cm<sup>-1</sup> which, according to the isotope rule, correspond with the hydroxyl bands. H–D exchange was effected by adsorbing  $D_2O$  at room temperature, followed by pumping at 823 K.

The relative intensities of these three bands proved to be a function of the  $\text{Re}_2\text{O}_7$  content; the lower this content, the higher the intensity of the type I band (Fig. 3).

As follows from Fig. 1 carrier and catalyst spectra are both characterized by bands at 2344 and 1380 cm<sup>-1</sup>. The bands at 2344 cm<sup>-1</sup> can be assigned to CO<sub>2</sub> in closed pores of Al<sub>2</sub>O<sub>3</sub> aerogel, and are characteristic for spectra of this type of material (19). The origin of the band at 1380 cm<sup>-1</sup>, which has also been observed in spectra of other types of alumina, is not



FIG. 5. Adsorption of  $H_2O$  on a  $Re_2O_7/Al_2O_3$  catalyst at ambient temperatures. (a) Base spectrum and (b) and (c) after adsorption of increasing amounts of  $H_2O$ .

clear (20, 21). No further attention has been paid to these bands because they showed no change in shape and position during the experiments.

A remarkable feature of the Re<sub>2</sub>O<sub>7</sub>/Al<sub>2</sub>O<sub>3</sub> catalyst is a band at 2000 cm<sup>-1</sup> with a shoulder at 1980 cm<sup>-1</sup>. The latter band shifted to 1900 cm<sup>-1</sup> on reduction of the catalyst with hydrogen (773 K, 1 hr,  $27 \times 10^3$  Pa), followed by oxidation with <sup>18</sup>O<sub>2</sub> (723 K, 1 hr, 52 × 10<sup>3</sup> Pa) (Fig. 4). Deuteration of the catalyst had no effect on these bands.

## 2. Adsorption of Water

Figures 5 and 6, respectively, show  $H_2O$ and  $D_2O$  adsorbed at 307 K on the  $Re_2O_7/$ 

 $Al_2O_3$  catalyst, calcined in the standard way. The first spectrum shows a band at ca. 1620  $\text{cm}^{-1}$ , which can be assigned to a  $H_2O$  deformation vibration (22) and thus indicates associative adsorption. The extremely broad band centered around 3100 cm<sup>-1</sup> should then be due to hydroxylstretch vibration of associatively adsorbed  $H_2O$ . The results of  $D_2O$  adsorption experiments (Fig. 6) are in agreement with this view, as follows from the isotope rule. Figure 6 shows also that the shape of the original hydroxyl bands is hardly influenced by the adsorbed  $D_2O$ ; evidently adsorption does not occur through hydrogen bonding between the surface hydroxyl



FIG. 6. Adsorption of  $D_2O$  at ambient temperatures on a  $Re_2O_7/Al_2O_3$  catalyst. (a) Fresh catalyst and (b), (c), and (d) increasing amounts of adsorbed  $D_2O$ .



FIG. 7. Desorption and dissociation of adsorbed  $D_2O$ . (a) "Wet" catalyst, (b) to (e) after subsequent outgassing for 1 hr at 523, 573, 673, and 773 K.

groups and the D<sub>2</sub>O. A second feature of the spectrum is a small band at 2680 cm<sup>-1</sup>. Being close to the type II deuteroxyl band (2685 cm<sup>-1</sup>) it appears that associative as well as dissociative adsorption occurred. From adsorption-desorption experiments with catalysts at various temperatures it can be concluded that at higher temperatures dissociative adsorption increases.

Figure 7 shows the spectra of a deuterated catalyst on which  $D_2O$  is adsorbed at ambient temperature and next pumped at successively higher temperatures. It appears that, relatively speaking, type II and III deuteroxyl bands first increase in relative intensity, indicating dissociative adsorption, and only on pumping at higher temperatures (573-673 K) diminish. The decrease in intensity is presumably caused by condensation of the deuteroxyl groups. It is striking that type I deuteroxyl groups are not formed under these conditions. The character of this type of group is different from the two others, as is also indicated by the effect of the rhenium oxide content on the relative amount of these groups (Fig. 2).

## 3. Reduction of the rhenium heptoxide/ alumina catalyst

Reduction and subsequent oxidation was studied by various techniques.

a. X-Ray diffraction. The diffractogram of the oxidic catalyst showed only lines attributable to the carrier. After reduction (H<sub>2</sub>, 773 K, 1 hr) the diffractogram showed rather weak lines at d = 2.39, d = 2.23 and d = 2.10 Å, indicating the presence of metallic rhenium (22). From line widths a mean particle diameter of  $15 \times 10^{-9}$  m was estimated.

b. Gravimetry. Weight changes were monitored with a microbalance. Treatment with H<sub>2</sub> (26 × 10<sup>2</sup> Pa) at 823 K resulted in a rapid decrease of weight. By repeated evacuation and treating with H<sub>2</sub> a stable reduction level was obtained. Approximately the original weight was readily obtained in O<sub>2</sub> (26 × 10<sup>2</sup> Pa) at the same temperature.

Assuming that weight increase is exclusively caused by oxidation of rhenium metal to  $\text{Re}_2\text{O}_7$ , a  $\text{Re}_2\text{O}_7$  content of 16% is calculated. However, activation analysis of this sample established a  $\text{Re}_2\text{O}_7$  content of 20%. Such discrepancies were also found for catalysts with different amounts of  $\text{Re}_2\text{O}_7$  and different methods of preparation (24).

c. Electron microscopy. Catalysts studied by this technique were prepared by impregnation of a commercial gamma alumina (Ketjen H.D.S. base) with an ammonium perrhenate solution. These catalysts contained about 12% Re<sub>2</sub>O<sub>7</sub>. Transmission electron micrographs of the oxidic catalyst did not differ from those of the carrier (Fig. 8).

It can therefore be concluded that, if  $\text{Re}_2O_7$  crystals are present, these crystals have mean diameters smaller than  $2 \times 10^{-9}$  m. The electron micrograph of the reduced



FIG. 8. Electron micrographs of (a) Al<sub>2</sub>O<sub>3</sub> and (b) a reduced Re<sub>2</sub>O<sub>7</sub>/Al<sub>2</sub>O<sub>3</sub> catalyst. Reduction was effected by reducing with hydrogen  $(1.0 \times 10^5 \text{ Pa})$  for 1 hr at 823 K. Thickness of the sections  $5 \times 10^{-8} \text{ m}$ . Magnification 250,000 ×.



FIG. 9. Partial reduction of a  $\text{Re}_2\text{O}_7/\text{Al}_2\text{O}_3$ catalyst. (a) before reduction and (b) after reduction with NH<sub>3</sub>. This reduction was effected by adsorbing NH<sub>3</sub> on the catalyst at ambient temperatures followed by pumping at successively higher temperatures up to 823 K.

catalyst clearly shows black spots which, in view of the results of the X-ray diffraction measurements, we assign to metal crystals of rhenium (Fig. 8). According to this micrograph, the mean diameter of these crystals is approximately  $15 \times 10^{-9}$  m.

d. Infrared spectroscopy. Catalysts when reduced had a zero transmission. A partial reduction was effected with  $NH_3$ : the catalyst was saturated with  $NH_3$  at ambient temperature and next pumped at successively higher temperatures up to 773 K. The resulting infrared spectrum is shown in Fig. 9.

The effect of reduction on the transmission is evident. The spectrum shows a relative decrease of the type II and III hydroxyl groups. Furthermore a band at  $3800 \text{ cm}^{-1}$  is shown. We assign this band to a hydroxyl group because the corresponding deuteroxyl band appeared in a similar experiment with a deuterated catalyst. Analogous results were obtained when the catalyst was reduced with CO at temperatures between 573 and 773 K.

After several reduction-oxidation cycles the infrared spectrum of the oxidic catalyst did not differ from the original one.

#### DISCUSSION

## 1. Structure

The absence of characteristic  $Al_2O_3$ hydroxyl groups in the infrared spectrum of the  $Re_2O_7/Al_2O_3$  catalyst indicates a complete coverage of the carrier surface with  $Re_2O_7$ .

With regard to the structure of the Re<sub>2</sub>O<sub>7</sub> layer on the carrier surface it is useful to take account of ideas on the structure of another metathesis catalyst,  $MoO_3/Al_2O_3$ . In the latter the presence of a monolayer has been stated by several authors (25-28). Its structure has been described as epitactic (25), or, in corresponding terms, it has been said that monolayer and carrier form a continuum (26). The question as to what kind of  $Re_2O_7$  layer is present may be answered by comparing the surface densities of the rhenium and molybdenum cations on the respective catalyst surface. Sonnemans and Mars (26) found a mean surface density of one molybdenum per  $17 \times 10^{-20}$  m<sup>2</sup> catalyst surface. A 26% Re<sub>2</sub>O<sub>7</sub>/Al<sub>2</sub>O<sub>3</sub> catalyst had a specific surface area of 195 m<sup>2</sup>/g, corresponding with a mean surface density of one rhenium ion per  $30 \times 10^{-20}$  m<sup>2</sup>. It is permissible to compare the catalysts because in both cases the preferentially exposed carrier surface is of the (100) type (18, 26). Considering now that the  $\text{Re}_2O_7/$  $Al_2O_3$  surface is completely covered with  $Re_2O_7$ , the low value of the rhenium cation surface density strongly suggests that the Re<sub>2</sub>O<sub>7</sub> is a monolayer.

The nature of this monolayer does not appear to be epitactic. This is suggested when one takes into account the large difference in surface densities with the relatively small difference in transition metal ion densities in bulk  $\text{Re}_2\text{O}_7$  and  $\text{MoO}_3$ , given one rhenium cation per  $66.7 \times 10^{-30}$  m<sup>3</sup> and one molybdenum cation per  $57.7 \times 10^{-30}$  m<sup>3</sup>, respectively (29). Furthermore, the structure of an epitactic monolayer by definition cannot depend on the amount of metal oxide on the carrier surface. On the  $\text{Re}_2\text{O}_7/\text{Al}_2\text{O}_3$  surface the relative amounts of hydroxyl groups depend on the  $\text{Re}_2\text{O}_7$  content of the catalyst, which can only be explained by assuming different structures with changing  $\text{Re}_2\text{O}_7$  content.

We suggest that the Re<sub>2</sub>O<sub>7</sub> layer on the carrier surface consists of small aggregates of Re<sub>2</sub>O<sub>7</sub>, and those catalysts with smaller amounts of Re<sub>2</sub>O<sub>7</sub> (20% or less) have atoms of the Al<sub>2</sub>O<sub>3</sub> surface layer exposed. In the arrangement of the Re<sub>2</sub>O<sub>7</sub> aggregates the row-like structure of the Al<sub>2</sub>O<sub>3</sub> (100) surface might be reflected.

## 2. Hydroxyl Groups

Under atmospheric circumstances metal oxide surfaces are as a rule covered with hydroxyl groups (30). On evacuation at higher temperatures water is formed through a condensation process and coordinatively unsaturated ions will be exposed on the surface (31). This process is reversible, as indicated in the following scheme:

By dissociative adsorption hydroxyl groups are formed in pairs. This is observed for the type II and III hydroxyl groups of the  $\text{Re}_2\text{O}_7/\text{Al}_2\text{O}_3$  surface. Type I hydroxyl group is not formed on adsorption of water. Therefore, this group is not part of a pair. The fact that the number of type I groups relatively increases with decreasing  $\text{Re}_2\text{O}_7$  content can be explained by assuming bonding of hydroxyl groups to Al ions

which are exposed between the  $\mathrm{Re}_2\mathrm{O}_7$  patches. For instance:

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We assume that the type II and III hydroxyl groups are bonded to Re<sup>7+</sup> cations. This is in accordance with the relative decrease of the amounts of type II and III groups on reduction of the catalyst.

## 3. Reduction Properties

A remarkable property of the catalyst is that on reduction Re crystals are formed; therefore, a sintering must occur, while on subsequent oxidation this Re is spread out again to a monolayer. This agrees with the idea that the 3800 cm<sup>-1</sup> band, which is observed in the infrared spectra of partial reduced catalysts, might be the 3800 cm<sup>-1</sup> band seen in the infrared spectrum of the carrier and, therefore, might be assigned to carrier hydroxyl groups. Such groups become possible when parts of the carrier surface are exposed on sintering.

The reduction to the metal is also remarkable in comparison with the reduction properties of  $MoO_3/Al_2O_3$  and  $WO_3/Al_2O_3$  catalysts. Under comparable reduction circumstances these supported transition metal oxides are only slightly reduced, while all the corresponding transition metal oxides in pure form are reduced to metals under the same conditions (hydrogen, 823 K, 1 hr) (27, 32). As far as a comparison is allowed this suggests a difference in the structures of the Re<sub>2</sub>O<sub>7</sub> and MoO<sub>3</sub> layers on alumina. This was previously suggested from the difference in the surface densities.

Our gravimetric data indicate only a partial reduction of the  $\text{Re}_2O_7$  in spite of a severe reduction procedure. This can be explained by assuming a distribution in bonding strengths between the Re atoms

and the  $Al_2O_3$  surface. Analogous results have also been reported for a  $MoO_3/Al_2O_3$  catalyst (27).

## 4. Bands at 2000 and 1980 cm<sup>-1</sup>

Finally we wish to draw attention to the bands at 2000 and 1980 cm<sup>-1</sup>. In view of its shift to 1900 cm<sup>-1</sup> on <sup>16</sup>O–<sup>18</sup>O exchange, the band at 1980 cm<sup>-1</sup> can be assigned to a rhenium-oxygen vibration. The results of our gravimetric experiments indicate that only part of the rhenium-oxygen bonds is broken on reduction. Therefore, it is possible that also the 2000 cm<sup>-1</sup> band is caused by such vibration. As metal-oxygen bonds generally (22) have frequencies in the region between 1000 cm<sup>-1</sup> these bands are probably caused by overtones.

It is interesting that also in the spectra of our  $MoO_3/Al_2O_3$  and  $WO_3/Al_2O_3$ catalysts bands have been found at 2004 and 2030 cm<sup>-1</sup>, respectively, suggesting a relationship in the structures of these catalysts (3).

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